



2014 PLM Conference, 2014.6.25, COEX

6/22/2014

Custody Metering System for Natural gas 3D Modeling Realization and Development Direction

Valmax Technology Corporation
Designed by J.I Jeon
VALMAX Technology Corporation

Agenda

- VALMAX TECHNOLOGY CORPORATION Introduction
- Instrumentation Division Introduction
- Custody Metering System Concept
- System Integration & Components
- Project Review
- Q & A



VALMAX TECHNOLOGY CORPORATION

VALMAX TECHNOLOGY CORPORATION

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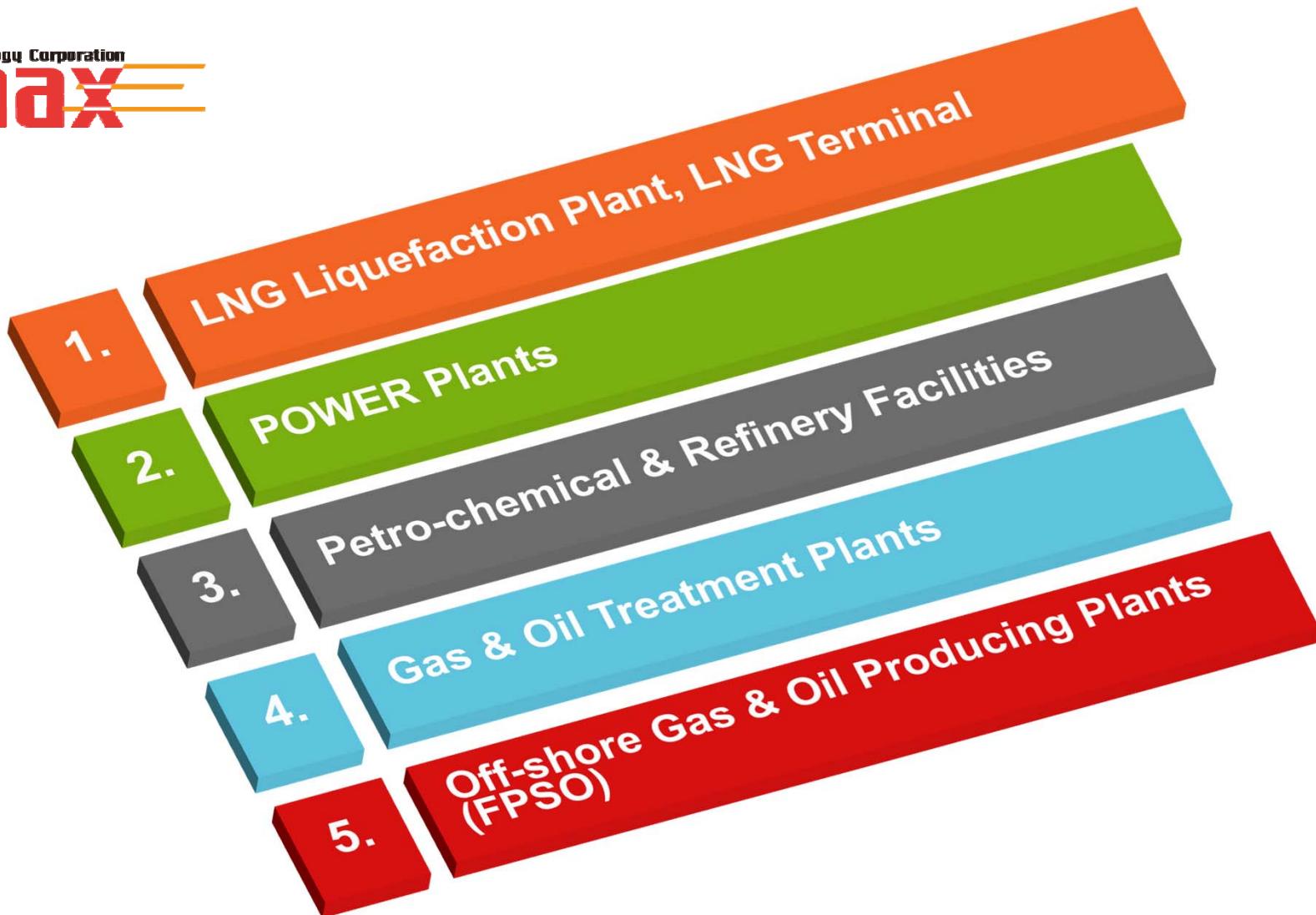
COMPANY OVERVIEW



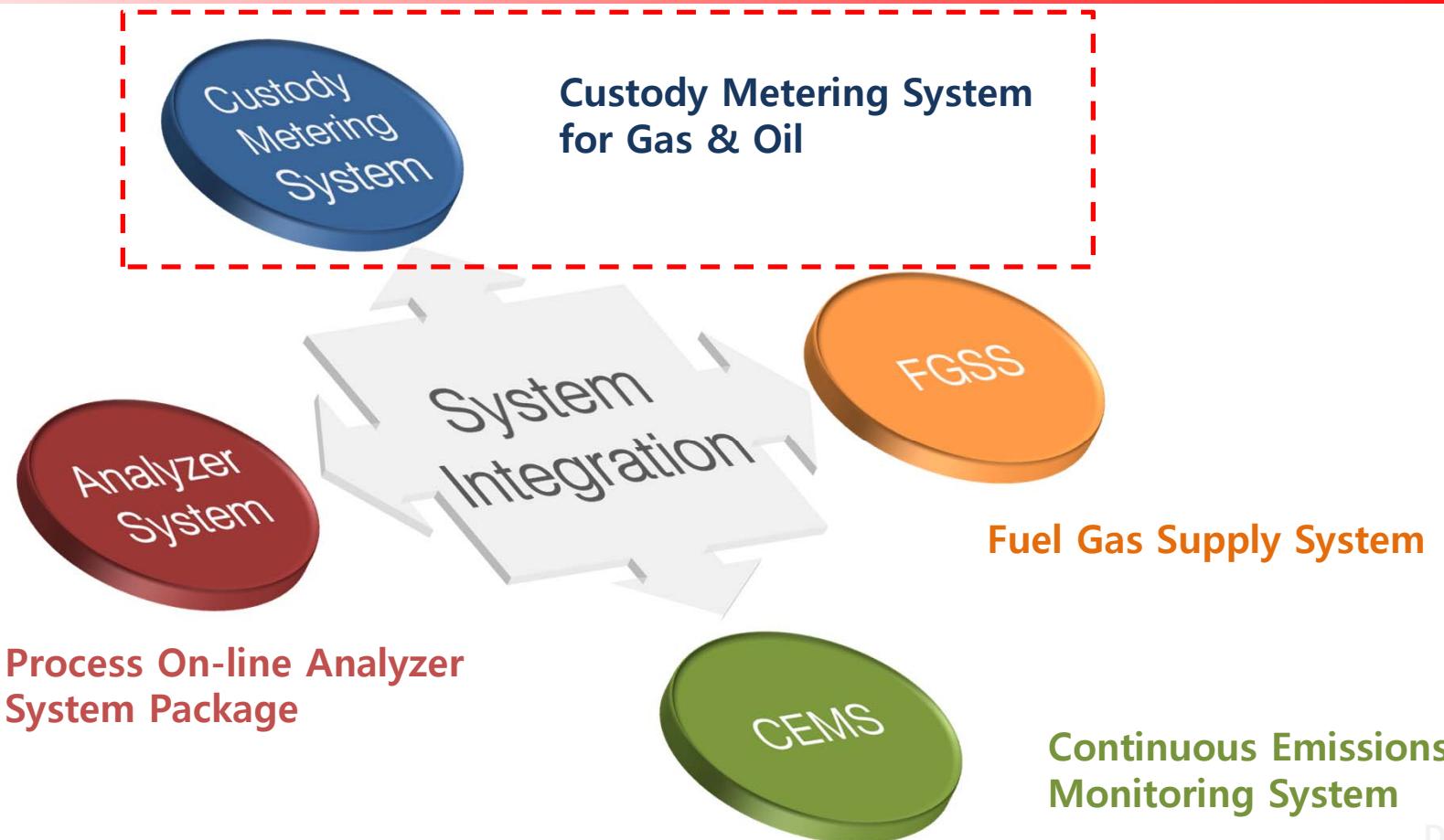
- Established : 6, December, 2002
- Nature of Business : System Integration,
Engineering Service
Product Representative
- CEO : Mr. Il-hwan kim



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System Integration



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Main Clients in KOREA



SAMSUNG HEAVY INDUSTRIES



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Main Clients in KOREA



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Main Clients in OVERSEAS



هيئة مياه و كهرباء أبوظبي
Abu Dhabi Water & Electricity Authority



إحدى شركات مؤسسة البترول الكويتية
A Subsidiary of Kuwait Petroleum Corporation

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INSTRUMENTATION DIVISION INTRODUCTION

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- 계측하는 범위가 넓고, 계량은 계측의 일부이며, 이러한 **계측 · 계량**을 하기 위해 **계측기류를 장비하는 것을 계장**이라 한다. 계장에는 계측기와 자동제어장치에 있어서 발신기, 수신기(지시계, 기록계, 증폭기 등), 조절부, 조작부, 공압(空壓)원, 유압(油壓)원 등 일체의 부착장비가 포함된다.

[네이버 지식백과] **계장** [instrumentation, 計裝] (산업안전대사전, 2004.5.10, 도서출판 골드)

1. Control

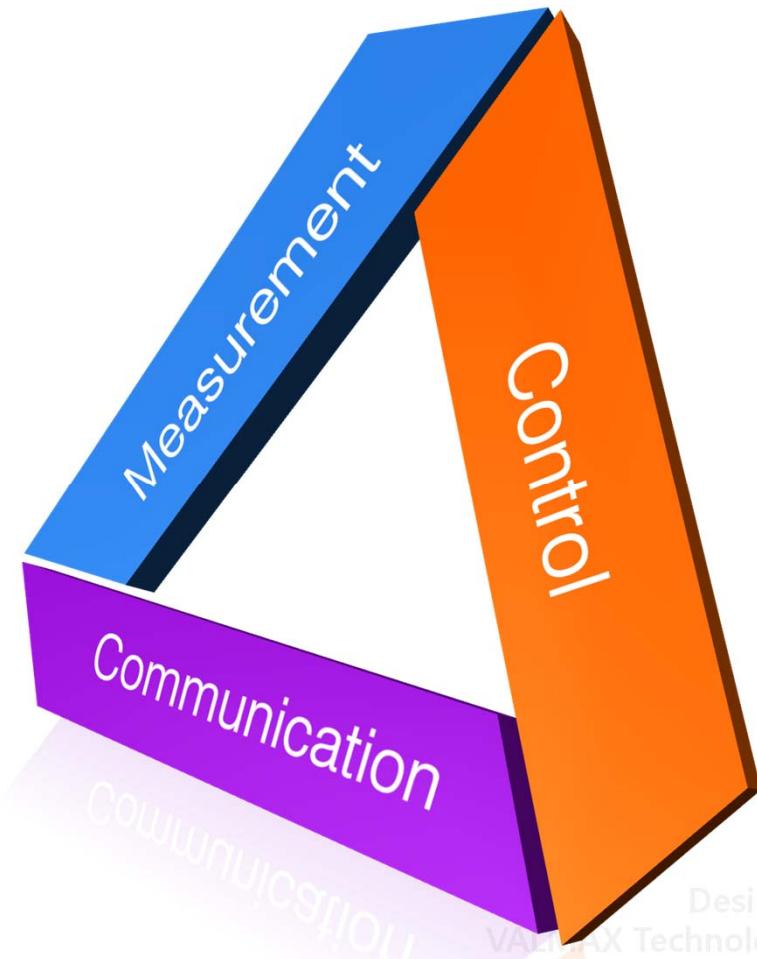
System Control

2. Measurement

Condition Measurement

3. Communication

Signal Communication among instruments



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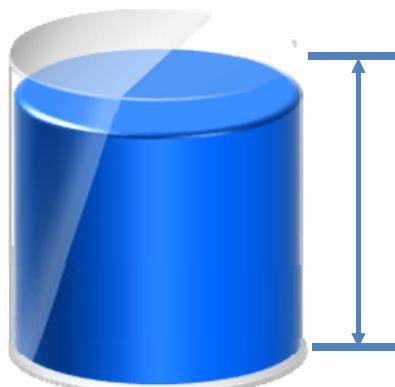


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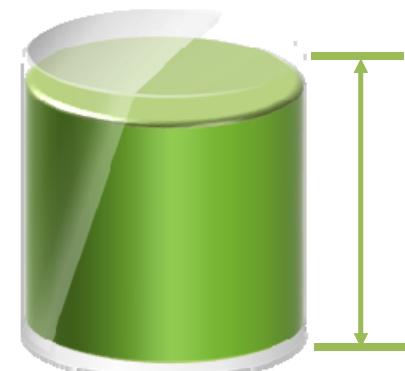
CUSTODY METERING SYSTEM CONCEPT

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For Example



100



100

본 페이지는 특정 브랜드의 광고를 위하여 제작한 것이 절대 아닙니다.

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Custody Metering System



- 정산용 계량 설비 및 System
- 발전소, 기타 플랜트에서 **비용**과 직결되는 가장 중요한 계장 설비 System
- 2012년 7월 1일부로 부피 거래제 -> **열량 거래제**로 변경, 시행 (국내 천연가스)

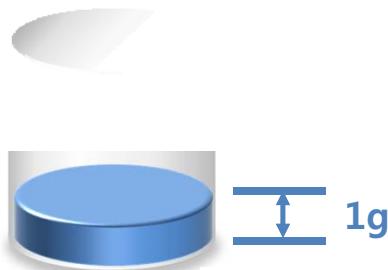


열량

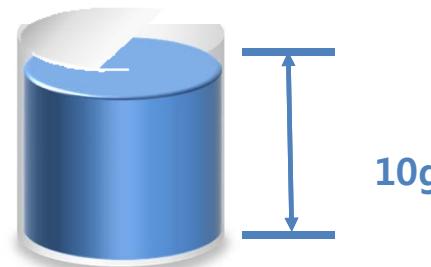
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열량? (Calorie Value)

- 물질의 온도를 높이는 데 필요한 열의 분량



온도를 1°C 올리기 위해서
1cal의 열이 필요하다

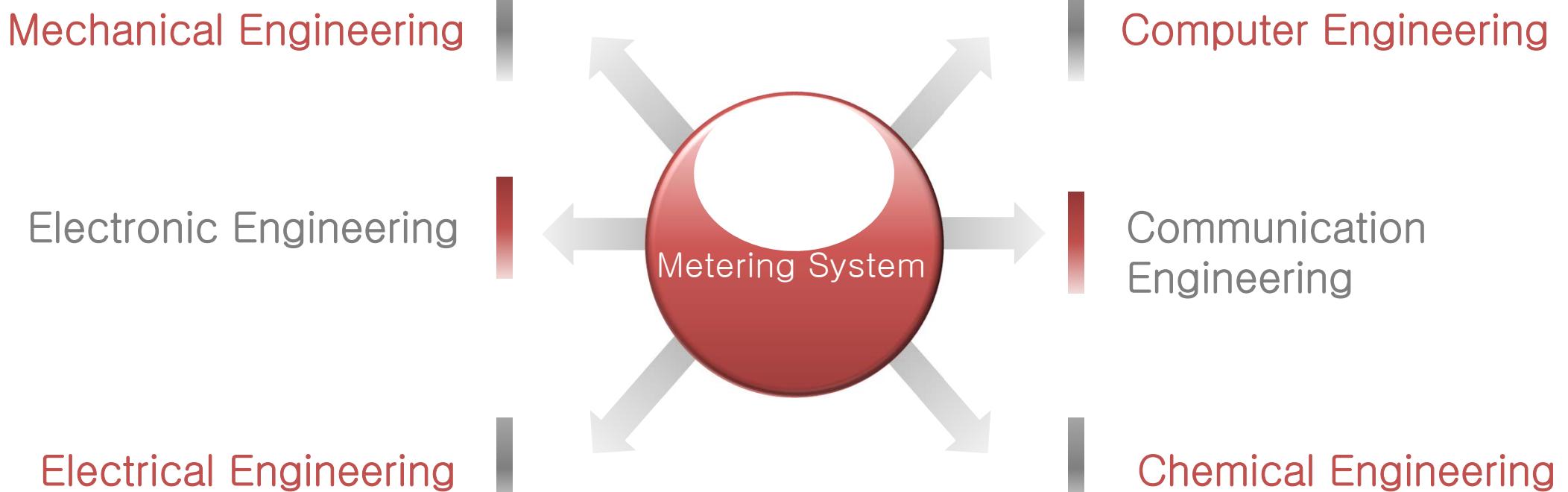


온도를 1°C 올리기 위해서
10cal의 열이 필요하다

Natural Gas와 열량과의 관계



- 열량이 높은 Gas = 좋은 Gas
- 열량 -> 발전소 간 비용 정산의 가장 중요한 거래단위
- 열량 측정 방법 = ISO 6976, AGA 8, GPA 2172
- 열량 계산 TOOL = FRCP, FRCPT, NGP



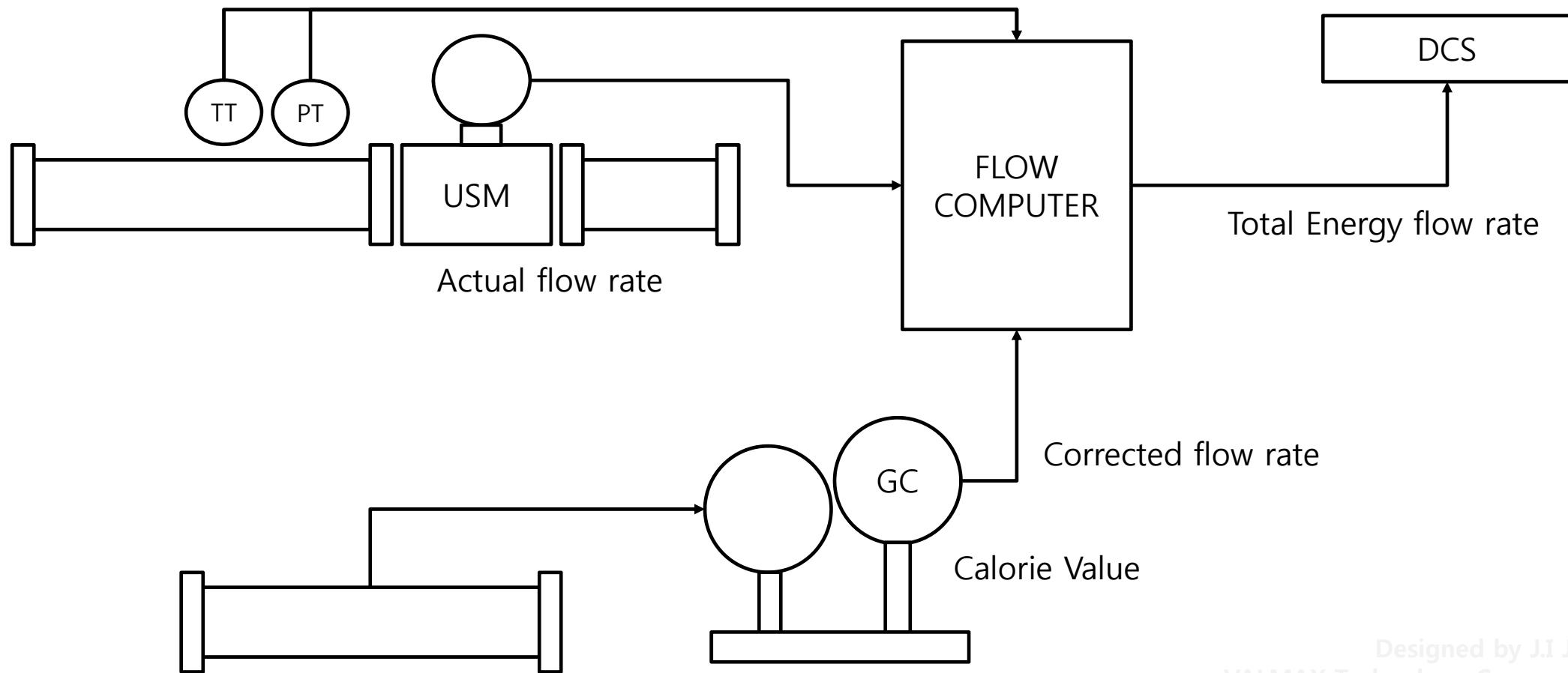


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SYSTEM INTEGRATION & COMPONENTS

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System Integration Diagram



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Flow rate Calc.

- 일반적으로 측정되는 유량
 - . Q_r : 유량계에서 흐르는 실제 체적유량 [m^3/hr]
 - . Q_b : 계약조건(101.325 kPa, 0 deg.C)에서의 보상 체적유량 [Nm^3/hr]
 - . Q_m : 질량유량 [Ton/hr]
 - . Q_e : 에너지유량 [GJ/hr]

Flow rate Calc.



각 유량의 상관 관계는 아래와 같다. (AGA-7, AGA-9)

- $Q_b = Q_r * (P_f / P_b) * (T_b / T_f) * (Z_b * Z_f)$
= $Q_r * (D_f / D_b)$
= $Q_m / D_b * 1000$
- $Q_m = Q_b * (D_b / 1000) = Q_r * (D_f / 1000)$
- $Q_e = Q_b * (E_d / 1000)$

- P_f : 현재 유체의 압력 [kPa]
- P_b : 계약 건 유체의 압력 조건 [101.325 kPa]
- T_f : 현재 유체의 온도 [deg.K]
- T_b : 계약 조건 유체의 온도 [0 deg.C = 273.15 deg.K]
- Z_f : 현재 유체의 압축계수 [Compressibility Authorize factor]
- Z_b : 계약 조건 유체의 압축계수 [Compressibility factor]
- D_f : 현재 유체의 밀도 [kg/m³]
- D_b : 계약 조건 유체의 밀도 [kg/Nm³]
- E_d : 계약 조건에서의 단위열량 [MJ/Nm³]

Flow rate Calc.

실체적 유량(Q_r)을 위와 같이 측정한다.

따라서

1. Q_r 로 Q_b 를 계산한다.(Z_b , Z_f 는 AGA8 로 계산)
2. Q_b 로 Q_m 을 계산 (AGA8 로 계산한 D_b 를 사용)
3. Q_b 로 Q_e 를 계산 (ISO6976 으로 계산된 E_b 를 사용)

앞의 계산에서 밀도의 오차는 유량에 직접적인 영향을 미침을 알 수 있다

밀도 값은 밀도계로 측정이 가능하나, 밀도계의 안정성 문제로 분석계기를 사용, 계산한 밀도를 사용한다.

분석계기를 사용한 밀도의 이론적인 계산 아래의 방법 계산한다.

D_f : AGA-8 Detailed or Gross Characterization Method (DCM/GCM)

D_b : AGA-8 Detailed or Gross Characterization Method (DCM/GCM)

단위열량은 아래의 방법으로 계산한다.

E_b : ISO6976 or GPA2172 등

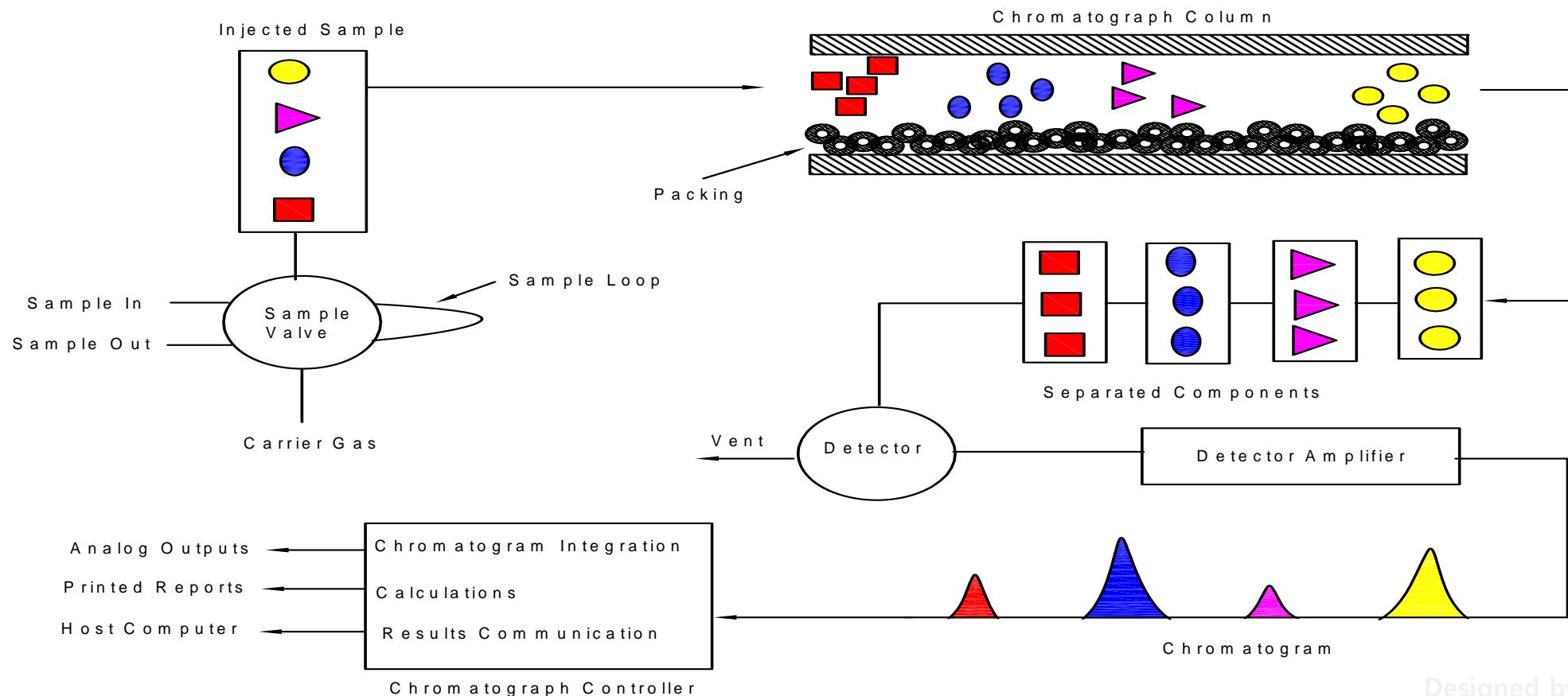
NGC 8206 Technical Description

Technology Corporation
Valmax



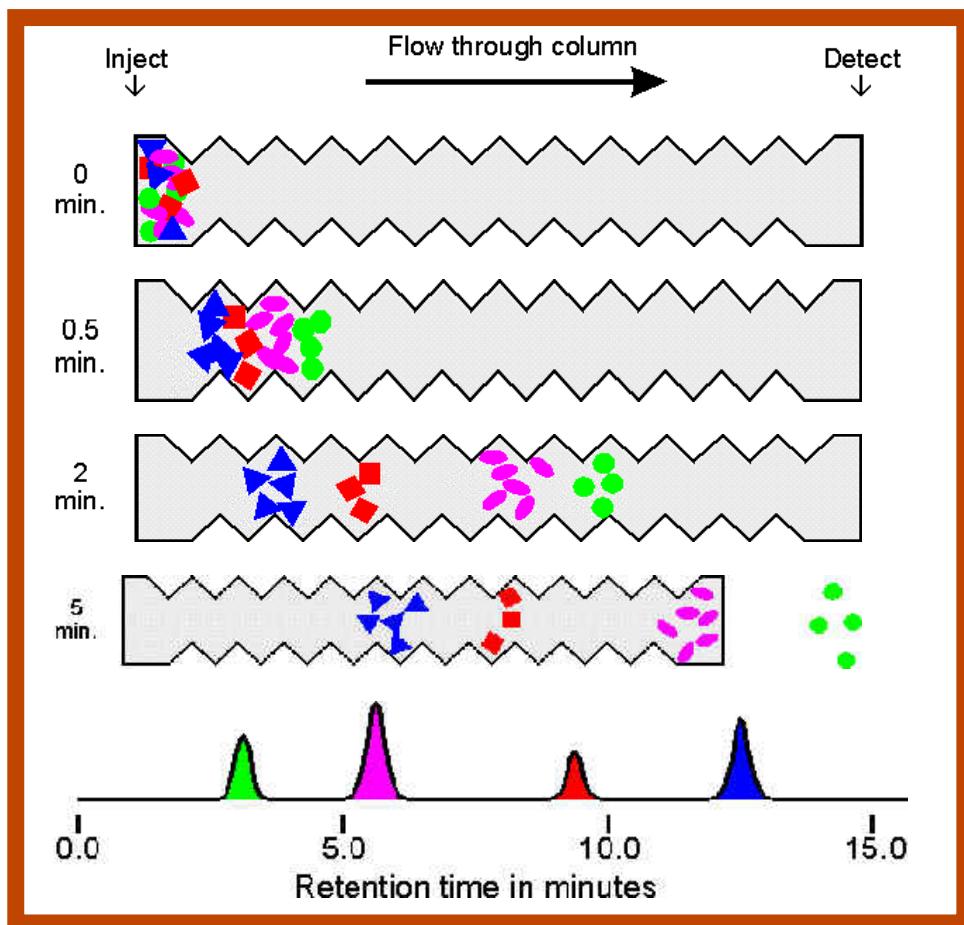
NGC 8206 Technical Description

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Valmax



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NGC 8206 Technical Description



This diagram shows a sample of natural gas with all the components lumped at inject (0 Min.)

The blue components have the highest absorption rate and the green components have the lowest.

The green components elute first and are detected first.

PCCU32 - [Entry]

Operate View Window Help

Enter COLLECT Operate NGC MB Setup

T120271394

- Communications
 - MMI Serial - COM0
 - TF Remote - COM1
 - Modbus/TCP Server, HMI
 - Totalflow TCP/USB
 - Modbus/TCP Server, DCS
 - Modbus/TCP Server, PLC
- PGC I/F - COM2
 - Setup
 - Communications
- NGC Server
 - Setup
 - Communications
- I/O Interface
 - EEPROM
- Analyzer Operation**
 - Cycle Control
 - GCM Main
 - Status & Graphs
 - Analog/Digital Comm
 - Diagnostics
 - Operation
 - GCM Aux
 - Status & Graphs
 - Analog/Digital Comm
 - Diagnostics
 - Operation
 - Chrom Processing
 - C3 - C6+
 - Peak Find
 - Peak Setup
 - Filters
 - N2 - C2
 - Peak Find
 - Peak Setup
 - Filters
 - H2S
 - Peak Find
 - Peak Setup
 - Filters
 - C6 - C9+
 - Peak Find
 - Peak Setup
 - Filters
 - STREAM1
 - Setup
 - Calculation Setup
 - Gas Factors
 - Alarms
 - Archive
 - Calibration

Operation Stream Sequence Cycle Schedule

Cycle Time: 6:10 / 6:40 07/17/2013 14:28:24

Sample Pressure -0.10 psig
 Col 1 Pressure 39.50 psig
 Col 2 Pressure 16.80 psig
 Oven Temp 140 deg F
 Enclosure Temp 103 deg F
 Supply Voltage 24.00 volts

GCM MAIN

Peak Find Calibration Diagnostics Alarm Logs Raw Chrome

Run Hold Cal

Stream 1 Stream 2 Stream 3 Stream 4

1 2 3 Cal

OK OK OK OK

UnNorm 108.25 133.90
 Superior (Dry) CV 1029.39 1106.32

Stream/Cal Chromatogram

Results Results Results Results

Setup Setup Setup Setup

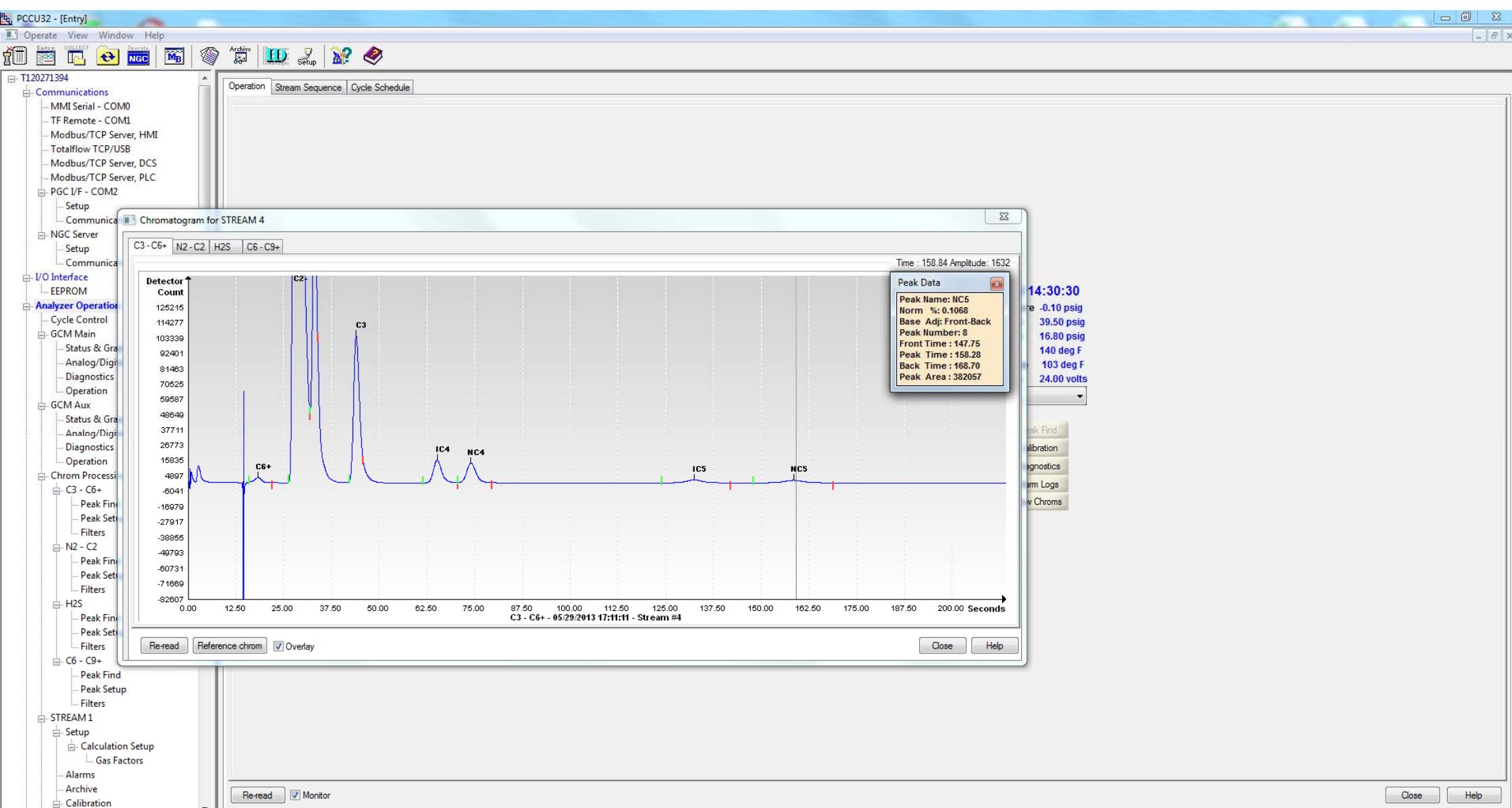
Stream ID STREAM 1 STREAM 2 STREAM 3 STREAM 4

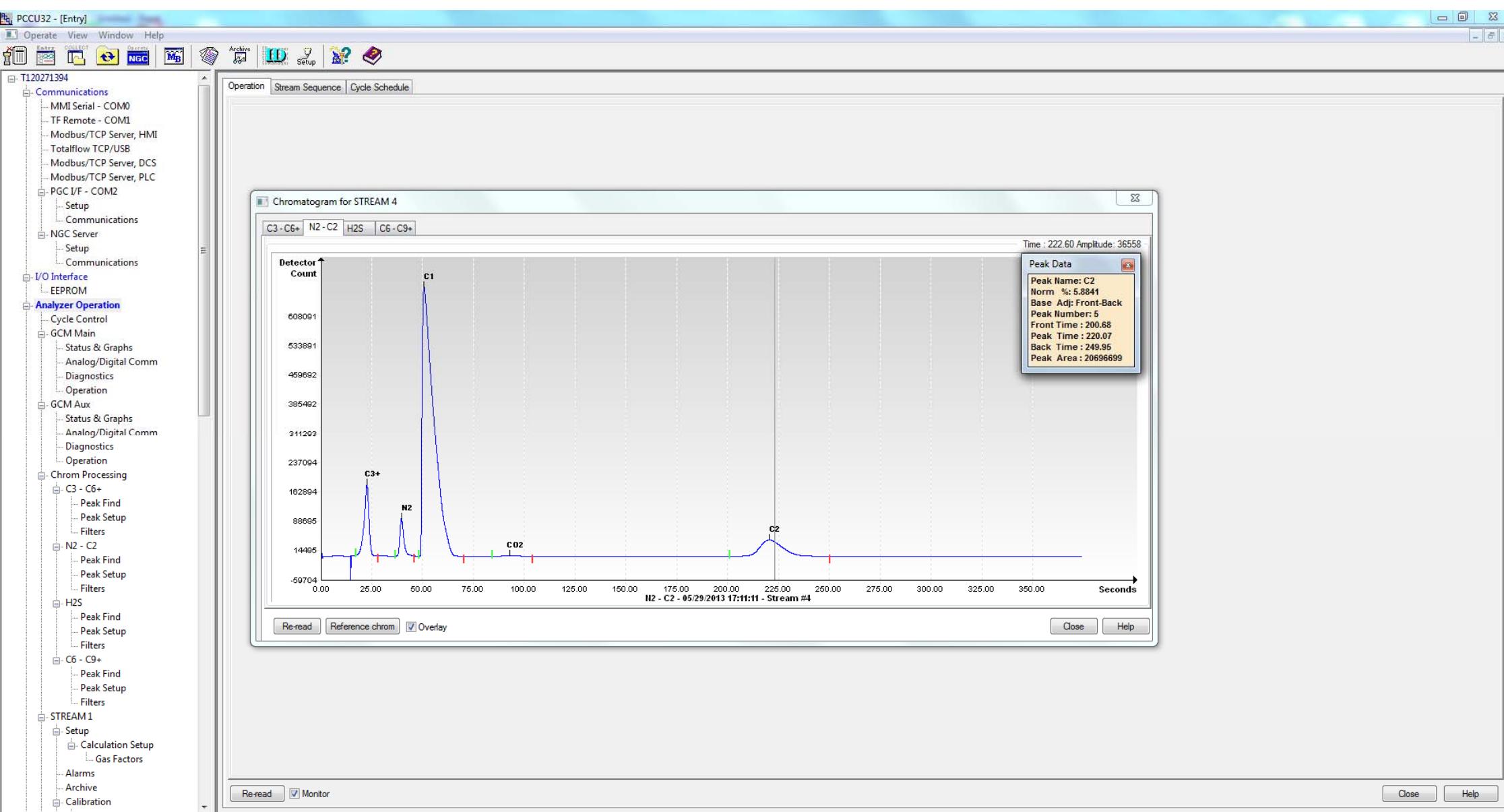
Active/Next Disabled Disabled Skip

Re-read Monitor

Reading Status

Close Help





Station ID: T120271394
Device ID : STREAM 4

Location: Location of Stream 4

SYSTEM:
LEASE:
OPERATOR:

STATE:
PRODUCER:
BUYER:

Results Date/Time 07/18/2013 09:19
Stream Number 4
Manifold Temp 85.997 (deg F)
Oven Temp 140.000 (deg F)
Calculation Type AGA-8
Stream Application Rev 2103501-007
Metrology Control Number 2103313-001
Flash Software Part Number 2103600-010
Contract Pressure 14.730 (psia)
Contract Temp 60.000 (deg F)
Carrier Pressure(1) 38.000 (psig)
Carrier Pressure(2) 16.800 (psig)
Sample Pressure 10.566 (psig)

Comp	Response Factor	UnNorm%	Norm%	P Area	Standard Concent.	Old.Resp Factor	%Response Difference
Propane	1.4667	3.1321	3.1300	19418560	3.1300	1.468	-0.0657
Hydrogen Sulfide	0.0000	0.0000	0.0000	0	0.0000	0.720	0.0000
IsoButane	2.5796	0.5318	0.5320	1747061	0.5320	2.579	0.0304
Butane	12.9472	0.5154	0.5110	1464565	0.5110	13.059	-0.8545
NeoPentane	0.0000	0.0000	0.0000	0	0.0000	0.647	0.0000
IsoPentane	0.4387	0.1060	0.1063	399405	0.1063	0.437	0.3277
Pentane	2.1043	0.1064	0.1064	404365	0.1064	2.104	0.0324
Hexane+	0.0000	0.0000	0.0000	0	0.0000	0.308	0.0000
Nitrogen	4.1497	3.2238	3.2300	8358918	3.2300	4.142	0.1884
Methane	1.1677	86.3285	86.3296	177653465	86.3296	1.168	0.0012
CarbonDioxide	1.1941	0.1012	0.1015	316563	0.1015	1.191	0.2537
Ethane	0.9460	5.8891	5.8900	20840160	5.8900	0.946	0.0156
Hexane	0.9266	0.0319	0.0321	346417	0.0321	0.921	0.5808
Heptane+	0.0000	0.0000	0.0000	0	0.0000	0.000	0.0000
Heptane	0.8302	0.0103	0.0105	126468	0.0105	0.817	1.5957
Octane	0.8363	0.0097	0.0104	124353	0.0104	0.783	6.8772
Nonane+	0.8398	0.0000	0.0000	121461	0.0102	0.000	100.0000
Nonane	0.0000	0.0000	0.0102	0	0.0000	0.000	0.0000
Decane	0.0000	0.0000	0.0000	0	0.0000	0.000	0.0000
Undecane	0.0000	0.0000	0.0000	0	0.0000	0.000	0.0000
Dodecane	0.0000	0.0000	0.0000	0	0.0000	0.000	0.0000
Ethane-	0.0000	0.0000	0.0000	0	0.0000	0.000	0.0000
Propane +	0.0000	0.0000	0.0000	0	0.0000	0.000	0.0000
Total	99.9863	100.00		100.0000	100.0000		



Calibration Report 출력

교정 가스 값을 기준으로 각 조성 비율 측정

Flow Computer

- 신호의 수신, 변환, 유량계산 (순시 값, 적산 값), 데이터 저장
- REDUNDANCY SYSTEM으로 통상적으로 구성
- 센서신호로부터 물리적 값으로 전환하여 **유량 값을 계산**
- **0°C 1 기압 또는 15 °C 1 기압 으로 물량 값 보정 계산**



Flow Computer



- 계산 값 확인을 위하여 FRCPT 또는 FRCP Program 사용
- 입증 테스트 시 오차율은 $\pm 0.02\%$ 임

PCCU32 - [Entry]

Operate View Window Help

BYEOLLAE

- Communications
- I/O Subsystem
- Units Conversion
- Holding Registers
- Operation
- BYEOLLAE
- Analysis
- Aux Contacts
- No Flow
- Units
- Therms Master
- Data
- Trend System
- Display
- Station
- Station ID
- Battery Voltage
- SU AGA7
- Static Pressure
- Temperature
- Mass Flow Rate
- Vol Flow Rate
- Last Calc. U-Vol
- Last Calc. Vol.
- Meter Input
- Yesterday Volume
- Accum. Energy
- Accum. Volume

General Constants Factors Limits Fixed Values On Errors Commands Log Capacity Current Values Last Calc Values

Description	Value	Units
Current Values		
11.7.9 Static Pressure (Grp 2)	269.460	kPa
11.7.80 Temperature (Grp 5)	31.140	deg C
11.7.0 Pulse Count	417	Counts/Flow Period
11.7.6 Flow Rate (Grp 20)	3146.372	Nm ³ /hr
11.7.10 Uncorrected Flow Rate (Grp 25)	125.100	Nm ³ /hr
11.7.36 Mass Flow Rate (Grp 15)	2.459	tonnes/hr
11.7.37 Energy Flow Rate (Grp 30)	134.578	GJ/hr
Today's Values		
11.7.7 Volume (Grp 18)	5.583	Nm ³
11.7.11 Uncorrected Volume (Grp 23)	0.222	Nm ³
11.7.74 Mass (Grp 13)	4.365	tonnes
11.7.77 Energy (Grp 28)	238.818	J
Yesterday's Values		
11.7.9 Volume (Grp 18)	1.488	Nm ³
11.7.13 Uncorrected Volume (Grp 23)	0.056	Nm ³
11.7.75 Mass (Grp 13)	1.163	tonnes
11.7.78 Energy (Grp 28)	63.646	J
Accumulated Values		
11.7.8 Volume (Grp 18)	12.603	Nm ³
11.7.12 Uncorrected Volume (Grp 23)	0.492	Nm ³
11.7.73 Mass (Grp 13)	10.029	tonnes
11.7.76 Energy (Grp 28)	544.735	J
Last Calculated Values		
11.7.33 Volume (Grp 16)	0.052	Nm ³
11.7.34 Uncorrected Volume (Grp 21)	0.002	Nm ³
11.7.45 Mass (Grp 11)	40.876	tonnes
11.7.46 Energy (Grp 26)	2.237	J

Re-read

Ready

DOSBox 0.74, Cpu speed: 3000 cycles, Frameskip 0, Program: FRCP_TB -

Files Declare Entry_Value Density Run \DEFAULT.FUN\ Yes

<<< PROGRAM OUTPUT >>>

Uncorrected volume flow rate, qb	:	125.10 Nm ³ /h
Uncorr. volume flow rate(linearised), qb-c	:	
Corrected volume flow rate, qn	:	3146.6 Nm ³ /h
Mass flow rate, qM	:	2.4598 ton/h
Energy flow rate, qE	:	32.1670 Gcal/h
Average fluid velocity in pipe	:	1.9050 m/s
Current compressibility, z	:	0.947690047
Normalized compressibility, zn	:	0.997112194

Error을 계산

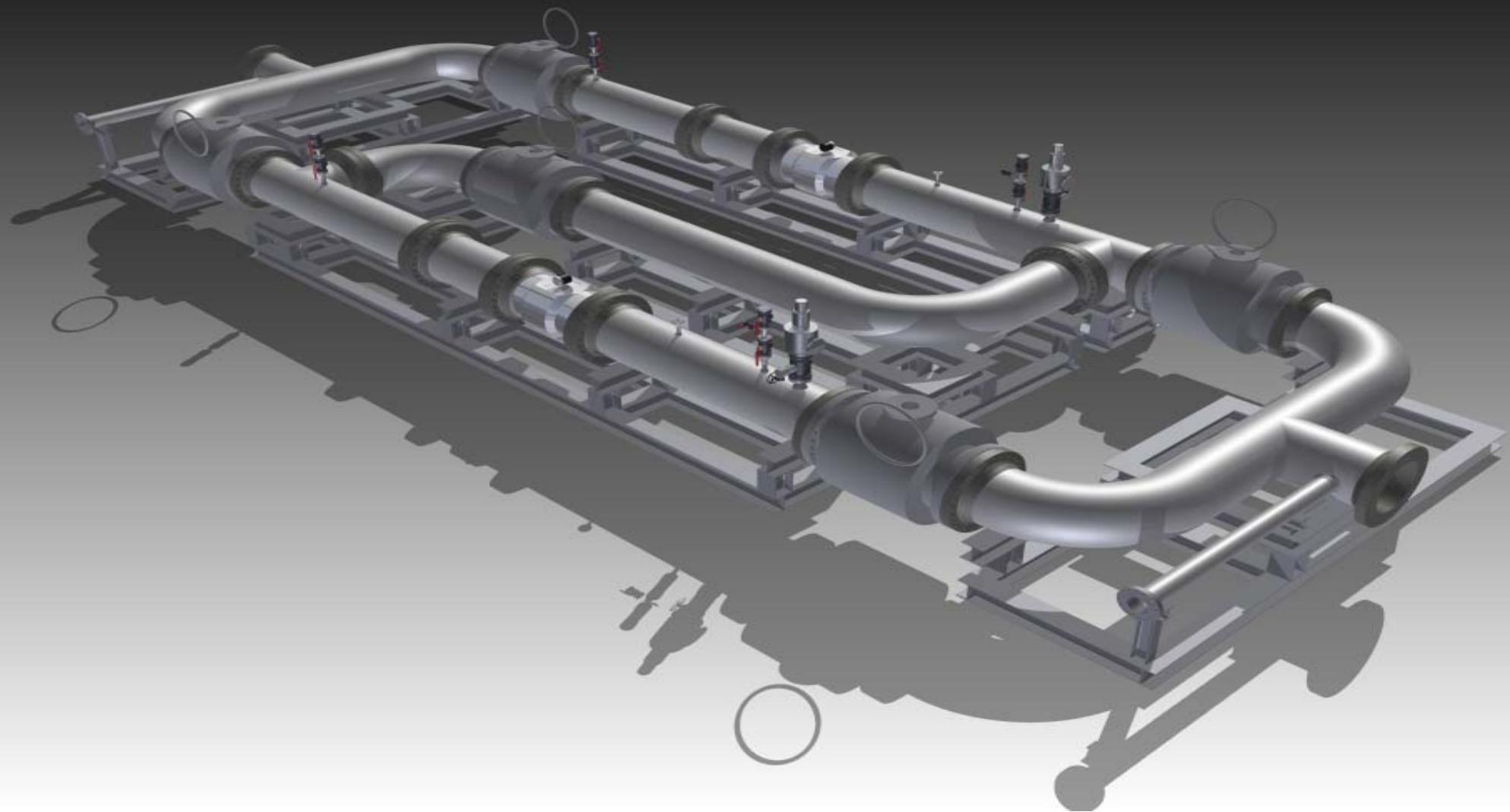
16:54	Volume Flow Rate (Nm ³ /h)	Mass Flow Rate (ton/h)	Energy Flow Rate (GJ)		Pulse
Flow Computer	3146.372	2.459	134.578		417
FRCPT	3146.6	2.4598	32.167	4.184	83.4
			134.586728		
Error	0.007245916	0.032522969	0.027133398		



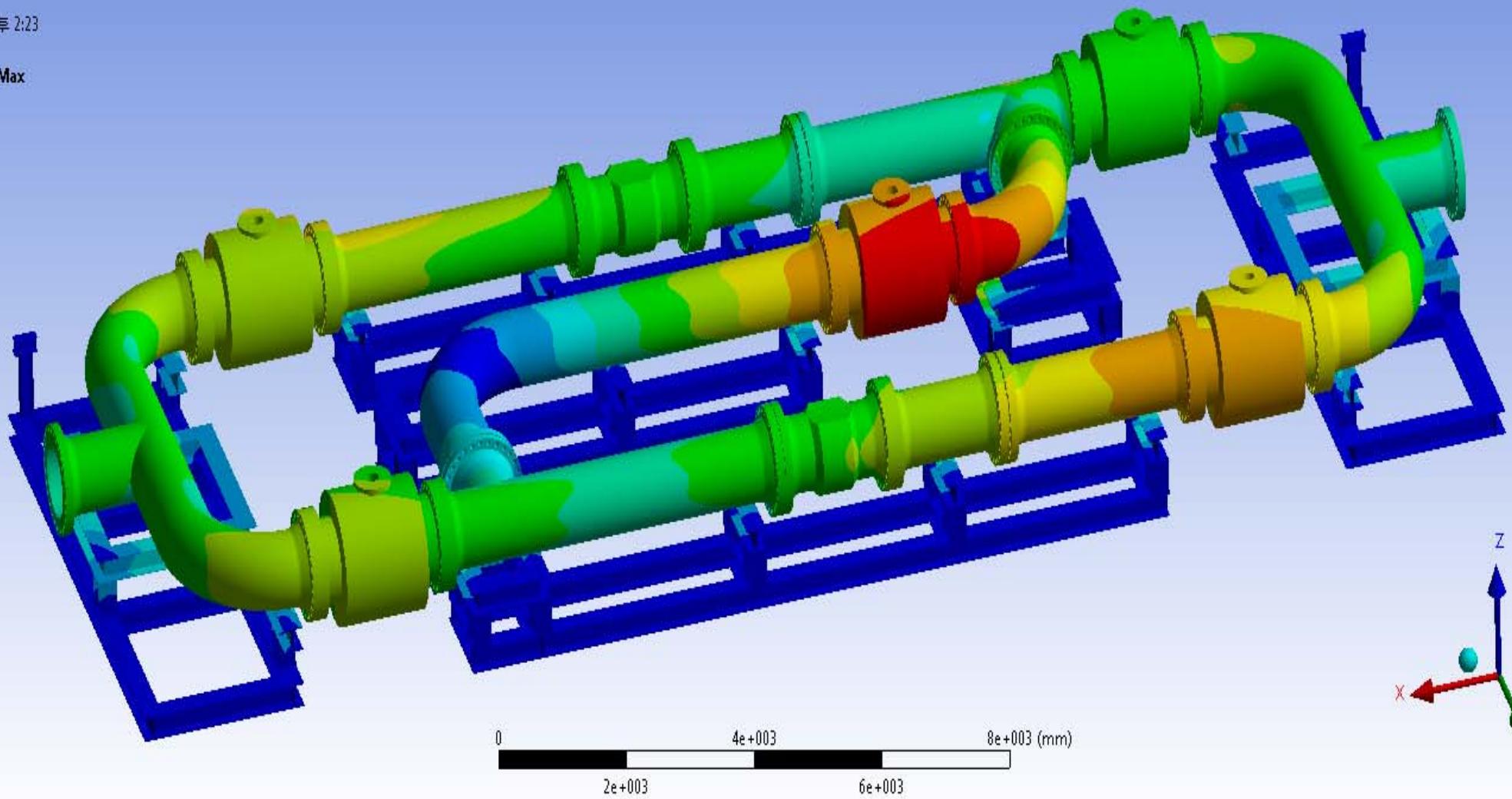
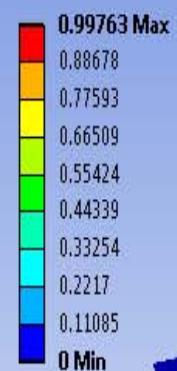
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PROJECT REVIEW

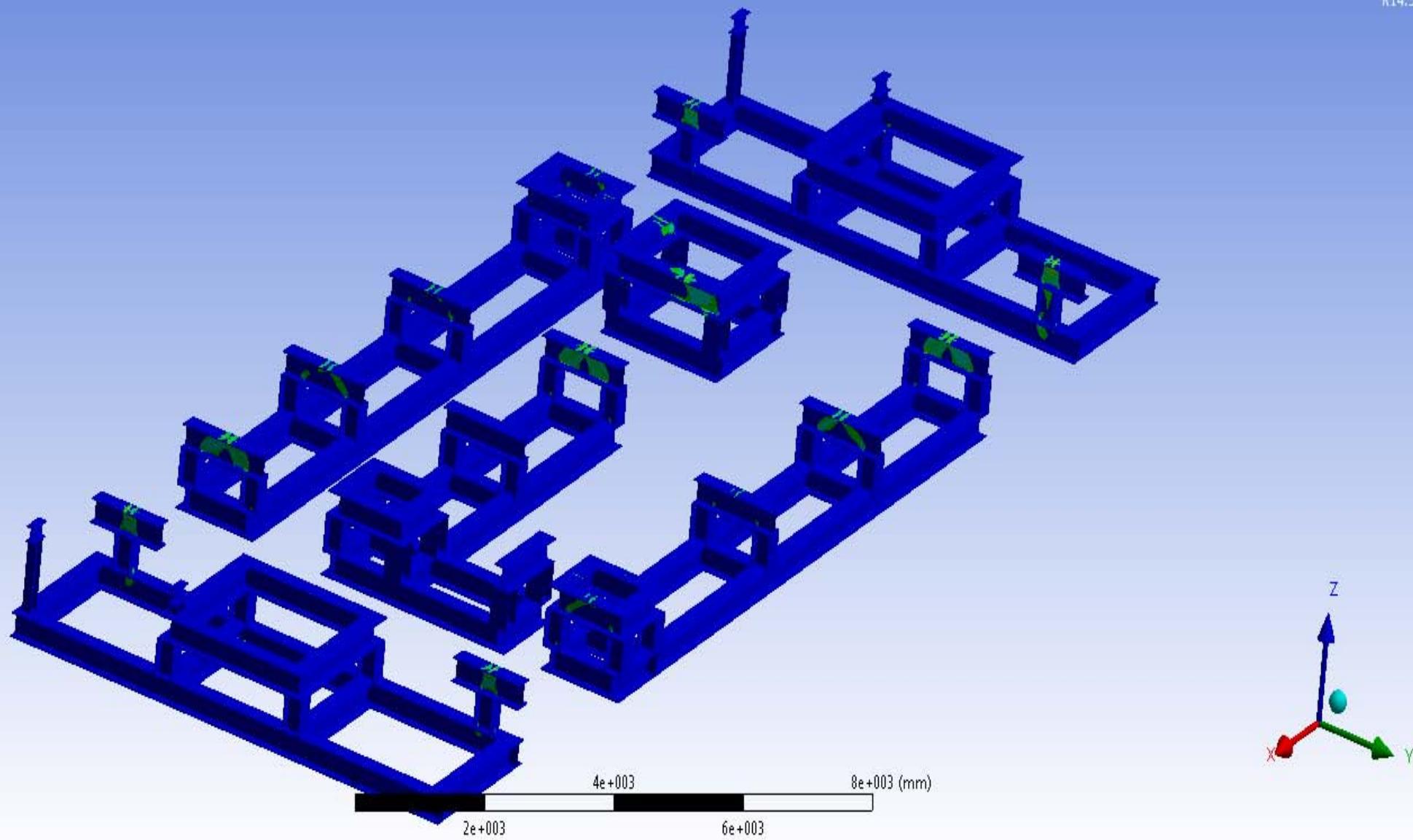
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A: Static Structural
Total Deformation
Type: Total Deformation
Unit: mm
Time: 1
2013-02-05 오 2:23

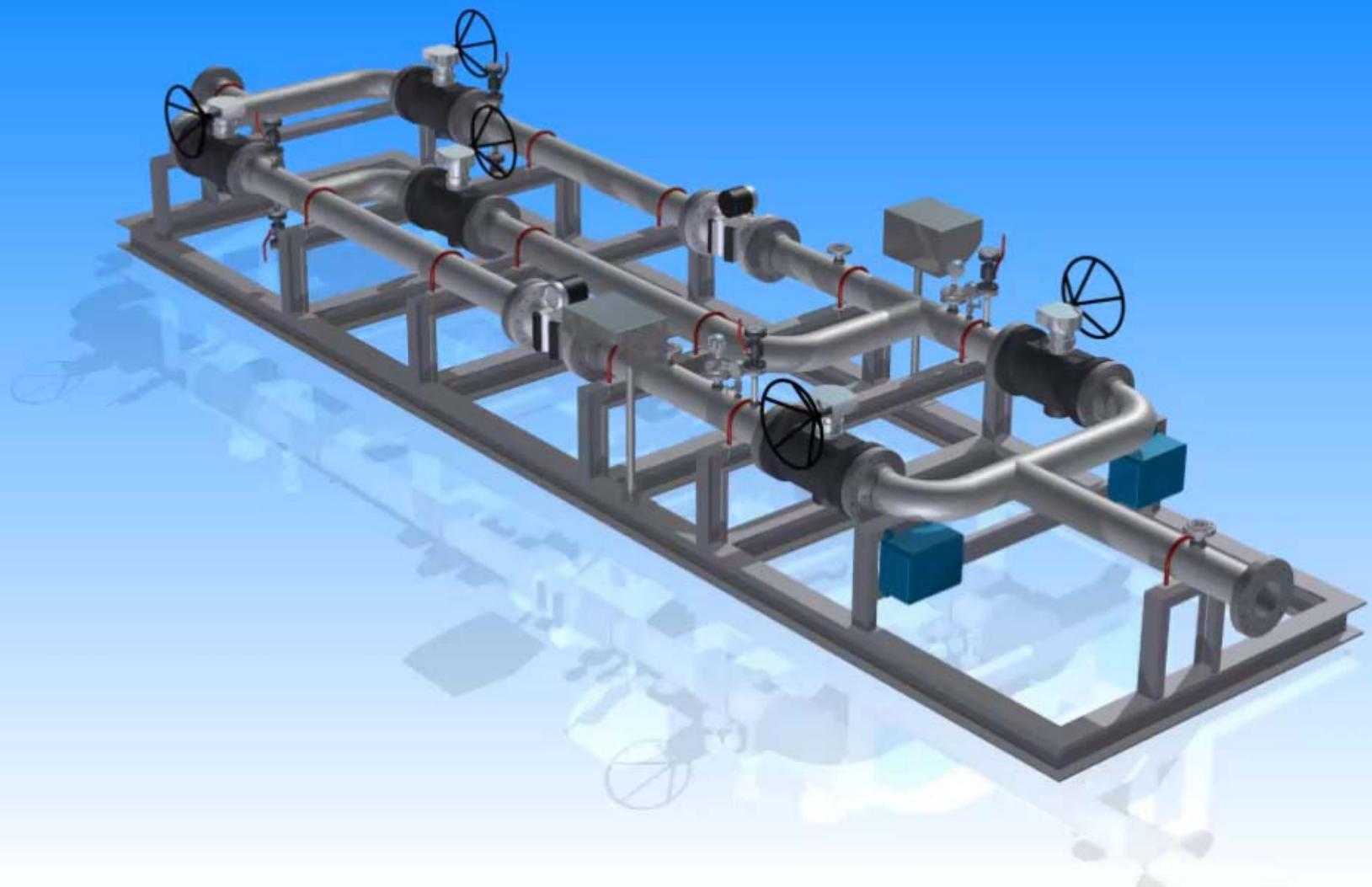


A: Static Structural
Safety Factor
Type: Safety Factor
Time: 1
2013-02-05 오후 2:25









QUESTIONS & ANSWERS



Thank you for attention

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